

**APPENDIX A**  
**SUPPORT FOR AMENDED AND NEW CLAIMS**

Claims	Nature Of Change/Recitation	Supporting text in Patent
3, 6, 10, 12, 15, 26, 31, 35, 41, 53-56, 63, 65	Formal (non-substantive) changes only	
4	partial recovery of working fluid	col. 8, lines 4-16; col. 15, lines 38-48
9	changing “weight” to <i>mass flow</i>	Table 3; col. 19, lines 27-28
14	deletion of ‘while the entropy of the engine held substantially constant’	entropy is a physical property, not a structural element, and in any event, constant entropy is not realizable in a physical system
18	deletion of “are cooled substantially, solely by the latent heat of vaporization of water”	col. 12, lines 32-44; col. 16, lines 18-28; col. 20, lines 56-67
20	deletion of “at the pressure of the combustion chamber without additional work for compression and without additional entropy”	see reference relative to claim 14
21	working fluid comprises . . .	original wording excluded pollutants, which are present to some degree
23	<i>to deliver fuel into</i> the combustion chamber	col. 8, lines 59-64
30	igniter	col. 10, line 42
32	downstream compressor	col. 8, lines 11-16
43	changing “controlled . . . vaporization of such water” to <i>controlled substantially by way of such water</i>	col. 12, lines 32-44; col. 16, lines 18-28; col. 20, lines 56-67
46	unburned	col. 1, lines 17-22; col. 12, lines 12-15; col. 17, lines 7-14; col. 19, lines 41-42

Claims	Nature Of Change/Recitation	Supporting text in Patent
52	deletion of “engine”	col. 1, lines 17-26; col. 5, lines 21-23; col. 24, lines 1-8
52	changing “fed in a fixed ratio . . . providing air” to <i>provided</i>	various fuel to air ratios are contemplated (see Table 3, line 4)
52	deletion of “having a pressure at least as great as the pressure of the compressed air”	deleted phrase is inaccurate (would preclude entry of the compressed air)
52	liquid <i>thermal diluent</i>	i.e., water; see also claim 1 (vaporizable non-flammable liquid); col. 17, lines 14-20
52	deletion of “the liquid prior to being injected . . . into the combustion temperature”	deleted clause is redundant
52	changing “the injected inert liquid . . . entering the combustion chamber” to <i>the injected liquid thermal diluent rapidly becoming a vapor upon entering the combustion chamber</i>	the term “flashing . . . immediately” implies an instantaneous event which is physically unrealizable. In practice, milliseconds are involved (col. 22, lines 40-42)
57	thermal diluent	see reference relative to claim 52
58, 60	air	see claim 1 (other changes are non-substantive)
64	deletion of “substantially all of the control . . . of the water introduced into the combustion chamber”	see reference relative to claim 43; (other changes are non-substantive)
75	deletion of “about constant” in clause (d)	various fuel to air ratios are contemplated (see Table 3, line 4)
75	changing “the water being converted substantially . . . to steam” to <i>at least part of the water being rapidly converted to steam upon entering the combustion chamber</i>	see reference relative to claim 52
75	addition of “unreacted components of the air, etc.”	see reference relative to claim 46

Claims	Nature Of Change/Recitation	Supporting text in Patent
75	changing “ substantially all . . . the latent heat of vaporization” to <i>most . . . a change in enthalpy</i>	for “substantially all, etc. see reference relative to claim 52; regarding enthalpy, this a proper technical description for all heat changes.
75	changing “work engine” to <i>external piece of equipment</i>	non-substantive
77-79	(entire claims)	col. 5, lines 42-48
80	re-compressor	col. 8, lines 11-16
81	81%	see table 3, first col.; col 21, lines 25-35
82	second work engine	col. 22, lines 58-60
83	at least one temperature detector	col 9, lines 50-56
84	stoichiometric burning  temp. control substantially by vaporization . . .	col. 3, lines 20-24; col. 7, lines 39-47; col 9, lines 30-49  see reference relative to claim 43
85	heat exchanger, etc.	col. 9, lines 36-39
86	an energy conversion system	col. 1, lines 17-26; col. 3, lines 49-51; col. 5, lines 21-23
86	a source of oxygen-containing fluid;	i.e., air
86	a source of fuel;	see claim 1
86	a source of thermal diluent fluid	water; see also claim 1 (vaporizable non-flammable liquid); col. 17, lines 14-20
86	a combustor including a combustion chamber, at least one inlet, and an outlet;	Figs. 2-3; col. 8, line 17-col. 10, line 37
86	delivery devices [for] oxygen-containing fluid, fuel, and thermal diluent fluid	Figs. 2-3; Col. 8, line 17-col. 10, line 37
86	the combustor being operative . . . to generate an energetic fluid . . .	broader recitation of “working fluid” (see claim 1)

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86	a controller operative to control the delivery of oxygen-containing fluid, fuel, and thermal diluent fluid	See claim 1
86	so that at least one pollutant is below a desired concentration in the energetic fluid exiting the combustor outlet, and	See Table 3
86	to control temperature in the combustor,	See claim 1
86	utilization device [which receives the] energetic fluid	Broader recitation of a ‘work engine’ (col. 1, lines 17-26; col. 5, lines 21-23; col. 24, lines 1-8)
87	igniter	col. 10, line 42
88	substantial portion of the oxygen [in the oxygen-containing fluid] is consumed	e.g., 90% (see patent claim 64); 95% (see patent claim 13)
89	compressor	see claim 1
90	pressure of the oxygen-containing fluid is at least about four atmospheres.	see claim 1
91	delivery device for the thermal diluent is operative to atomize and inject a portion of the thermal diluent into the feed air	see col. 6, line 66-col. 7, line 4
92	mass flow of the energetic fluid exiting the combustor substantially exceeds the mass flow of the air through the compressor.	Table 3
93	air delivered to the combustor is at a pressure between about 4 to about 100 times ambient	col. 7, lines 53-55
94	first burner zone . . . at least one additional burner zone; a portion of the oxygen-containing fluid [is admitted] into the first burner zone, etc.	col. 8, line 17- col. 9, line 29

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95	first feed mechanism [admits] approx. 50% of the total available oxygen-containing fluid into the first burner zone;  second feed mechanism [admits] the remaining available oxygen-containing fluid into the one or more downstream burner zones.	col. 9, lines 11-29
96	third burner zone, fourth burner zone, etc.	see col. 9, lines 11-29
97	injectors for thermal diluent downstream of the fourth burner zone	see col 10 lines 30-35
98	at least one injector for delivering thermal diluent to the oxygen-containing fluid prior to introduction . . . into the combustion chamber.	col. 8, line 17- col. 9, line 29
99	plurality of injectors for . . . thermal diluent . . . downstream of all of the burner zones.	see col 10 lines 30-35; col. 20, lines 42-49
100	heat exchanger for heating the oxygen-containing fluid, etc	col. 8, line 65- col. 9, line 10
101, 104	water injector upstream of combustion chamber, etc.	col. 8, line 17- col. 9, line 29
102, 103	construction of combustion chamber and heat exchanger	col. 8, 17-col. 9, line 10
105	non-potable water; collection of inorganic materials	col. 22, lines 6-39
106	condenser	col. 22, lines 6-16
107	fuel-rich burning in first burner zone, etc.	col. 9, lines 30-49
108	distribution of oxygen-containing fluid	col. 9, lines 11-49
109	heat exchanger for heating the oxygen-containing fluid, etc	see reference relative to claim 100

Claims	Nature Of Change/Recitation	Supporting text in Patent
110	< 3ppm NOx	col. 19, lines 43-47
111	< 3ppm CO	col. 19, lines 43-47
112	energetic fluid contains insignificant levels of pollutants, etc.	col. 3, lines 20-24; col. 3, lines 44-48; col 19, lines 26-63
113	at least about 81% of the oxygen is consumed	see reference relative to claim 81
114	controlled air to fuel ratio	see patent claim 12; see reference relative to claim 84
115	control of temperature and temperature profile in combustor by injection of thermal diluent	col. 9, line 57-col.10, line 37
116	control of delivery of thermal diluent according to desired maximum flame temperature	col. 2, lines 14-23; col. 17, lines 7-28
117	desired mean exit temperature of energetic fluid	col. 9, line 57-col. 10, line 37; col. 20, lines 51-56
118	control of peak exit temperature independent of the rate of energy conversion	col. 6, lines 40-50
119	control of thermal diluent to constrain temperature, etc.	col. 3, lines 44-48; col 18, line 60-col. 20, line 35; Table 3
120	temperature control by control of delivery of thermal diluent	col. 2, lines 14-23; col. 9, line 57-col.10, line 37; col. 17, lines 7-28; col.
121	location of delivery of thermal diluent	col. 2, lines 14-23; col. 9, line 57-col.10, line 37; col. 17, lines 7-28
122	control of energetic fluid temperature independent of enthalpy flow rate	col. 2, lines 42-53; col. 15, lines 52-64
123	temperature below about 2600°F	col. 10, lines 18-30
124	CO of 758 ppm or less	Table 3
125	sufficient residence time above 1800°F	col. 10, lines 18-30

Claims	Nature Of Change/Recitation	Supporting text in Patent
126	energetic fluid temp. between 750°F and 2600°F	col. 7, lines 55-60; col. 10, lines 18-30
127	delivery of thermal diluent at axially spaced locations	col. 9, lines 63-65
128-132	locations of delivery of thermal diluent	col. 9, line 57-col. 10, line11
133	temperature of combustor outer wall below a desired value	col. 15, lines 13-28
134	mass flow of the energetic fluid exiting the combustor is substantially more than the mass flow of the oxygen-containing fluid delivered to the combustor.	Table 3; col. 19, lines 27-28
135	oxygen to fuel ratio in range of 100-124% of stoichiometric ratio	Table 3, col. 1
136	independent control of fuel, oxygen-containing fluid and thermal diluent	col. 4, lines 39-44
137, 138, 140-142	independent control of temperatures, and fluids	col. 2, lines 14-23; col. 4, lines 28-46; col. 17, lines 7-28; col. 19, line 64-col. 20, line 27
139	feedback control system etc.	col. 5, lines 13-17; col.7, lines 5-14
143	utilization device	patent claim 1
144	oil well, etc.	col. 5, lines 1-5
145	desalinization, generation of electricity etc.	col. 3, lines 3-13; col. 23, lines 45-49; col. 24, lines 1-12
146	recovery of thermal diluent	col. 8, lines 4-16; col.15, lines 38-51
147	amount of recovered thermal diluent is at least equal to the amount delivered to the combustor outlet.	col. 3, lines 14-17; col. 8, lines 4-16;
148	purification of thermal diluent	col. 23, lines 28-44
149	ratio of thermal diluent to fuel	Table 3; col. 10, lines 35-37

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150	multiple combustion chambers	col. 8, line 17-col. 9, line 49 (multiple fire zones)
151	multiple utilization devices	see reference relative to claim 82
152	at least one temperature detector	col 9, lines 50-56
153	mass flow of thermal diluent at least twice the mass flow of fuel	patent claim 35; Table 3; col. 19, lines 27-28
154	substantially complete burning  the temperature adjustment . . . by the vaporization of the thermal diluent.	col. 18, lines 60-64; col. 19, lines 31-42  see reference relative to claim 43
155	oxygen-containing fluid under pressure, etc.	see claim 1
156	oxygen-containing fluid [delivered] at a pressure between about 4 to about 100 times ambient pressure.	see reference relative to claim 93
157	temperature of an inner wall of the combustor is at least 1093° C (2000° F).	col. 16, lines 16-18
158	independently control so the energetic fluid exits the combustor at about a desired temperature.	col. 2, lines 14-23; col. 4, lines 28-46; col. 17, lines 7-28; col. col. 19, line 64-col. 20, line 27
159	controller is operative to control the ratio of oxygen containing fluid to fuel to have about a first selected value and to control the ratio of the thermal diluent to fuel to have about a second different selected value.	See Table 3
160	thermal diluent comprises essentially water.	col. 17, lines 14-20
161	delivering an oxygen-containing fluid, fuel, and a thermal diluent fluid to the combustor through one or more inlets;	col. 8, line 17-col. 9, line 49

Claims	Nature Of Change/Recitation	Supporting text in Patent
161	combusting at least a portion of the delivered oxygen and at least a portion of the delivered fuel to form a combusting fluid;	see patent claim 39
161	mixing the combusting fluid with thermal diluent fluid to form an energetic fluid comprising thermal diluent fluid, combustion products, any uncombusted fuel, and oxygen-containing fluid;	see patent claim 1
161	controlling the delivery of oxygen-containing fluid, fuel and thermal diluent fluid so that the energetic fluid exiting the combustor includes a pollutant content below a desired concentration, and to control temperature in the combustor;	See Table 3; col. 17, lines 7-28
161	delivering the energetic fluid through the combustor outlet to a utilization device.	Broader recitation of a ‘work engine’ (col. 1, lines 17-26; col. 5, lines 21-23; col. 24, lines 1-8)
162, 163	oxygen-containing fluid is delivered to the combustor at an elevated pressure (in the range of about four to one hundred times the ambient pressure)	col. 7, lines 53-55
164	oxygen-containing fluid is delivered to the combustor at a pressure in the range of about 22 to about 50 times the ambient pressure.	Table 1
165	maintaining the ratio of oxygen-containing fluid to fuel and the ratio of thermal diluent to fuel substantially constant.	col. 5, lines 42-54
166	fuel and oxygen are combusted in the combustion chamber.	col. 8, line 17-col. 9, line 49
167	energetic fluid is at least partially formed in the combustion chamber.	col. 10, lines 18-23; col. 20, lines 42-49

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168	including the step of insulating the enclosure from heat from the combustion chamber.	col. 10, line 50-col 11, line 15
169, 170	differential pressure between the combustor inlet for the oxygen-containing fluid and the outlet of the combustor is maintained at less than 3.5% of the pressure of the oxygen-containing fluid entering the combustor.	col. 10, line 50-col 11, line 15
171	quantities of oxygen-containing fluid and fuel delivered to the combustion chamber are selected to maintain a desired ratio of oxygen-containing fluid to fuel.	Table 3
172	at least about 90% of the available oxygen is consumed	Patent claim 64
173	ratio of oxygen to fuel is in the range of about 100 percent to about 200 percent of the stoichiometric ratio.	Table 3
174	ratio of oxygen to fuel is in the range of 101 percent to about 124 percent of the stoichiometric ratio.	Table 3,
175	controlling the ratio of thermal diluent fluid to fuel in accordance with changes in the ratio of oxygen to fuel.	col. 5, lines 42-54
176	controlling the ratio of thermal diluent flow to fuel flow to be greater than a desired value,	col. 17, lines 7-28
177	of maintaining the ratio of thermal diluent fluid to fuel to be at least 2:1 by mass	col. 4, lines 53-57
178	ratio of thermal diluent to fuel is maintained within a range of about 2 to 1 to about 16 to 1 by mass	col. 4, lines 53-57; col. 10, lines 35-37

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179	varying the ratio of thermal diluent to fuel oppositely to changes in the ratio of oxygen-containing fluid to fuel	col. 5, lines 46-48
180-183	[controlling delivery of oxygen-containing fluid to two or more burner zones]	col. 9, lines 11-49
184	mixing a controlled amount of thermal diluent fluid with the oxygen-containing fluid prior to combusting the oxygen-containing fluid with the fuel.	see col. 20, lines 42-49
185	injecting controlled amounts of the thermal diluent at multiple locations in the combustion chamber.	col. 8, line 17- col. 9, line 29
186	at least part of the thermal diluent fluid is delivered downstream of the combustion chamber.	col. 8, line 17- col. 9, line 29
187	part of the thermal diluent fluid is delivered upstream of the combustion chamber.	col. 8, line 17- col. 9, line 29
188-194		col. 9, line 57-col. 10, line11
195, 196	bringing the fluid downstream of the combustion chamber to a desired degree of equilibration.	col. 10, lines 23-30
197	fluid is delivered through the combustor outlet at a desired temperature.	col. 7, lines 15-35
198	controlling the temperature of at least one of the delivered fluids.	see claim 1
199	controlling the fluid temperature of the combusting fluid and/or the energetic fluid.	col. 7, lines 15-35; col. 9, lines 57-60

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200	delivery of the fluids is controlled so that a desired value is obtained for at least one of the peak temperature, the mean temperature, and the temperature profile of the fluid in the combustor.	col. 2, lines 14-23; col. 4, lines 44-46; col. 9, line 57-col.10, line 37; col. 17, lines 7-28
201	delivery of the fluids to the combustor is controlled to constrain the temperature of the energetic fluid to be between about 399°C (750°F) and about 1426°C (2600°F).	col. 7, lines 55-60; col. 10, lines 18-30
202	temperature of an outer wall of the combustor is below a desired value.	see ref. to claim 133
203	the delivery of the fluids is so controlled that the temperature of the fluid within the equilibration chamber is below about 1427°C (2600°F).	col. 10, lines 18-30
204	portions of the thermal diluent fluid are delivered at locations upstream and/or downstream of the location of peak temperature in the combusting fluid.	col. 9, line 57-col. 10, line11
205	measuring fluid temperatures determining one or more of the mean temperature, peak temperature, and temperature profile	col. 2, lines 14-23; col. 4, lines 44-46; col. 7, lines 5-23; col. 9, line 57-col.10, line 37; col. 17, lines 7-28
206	[measuring fluid temperatures]	col. 7, lines 5-23; col. 20, lines 51-55; col. 23, lines 18-21
207	maintaining the temperature of the energetic fluid substantially at a desired value while varying the enthalpy flow rate of the energetic fluid.	See reference relative to claim 122.
208	controlling the ratio of thermal diluent fluid to fuel according to changes in the ratio of oxygen-containing fluid to fuel to obtain a desired energetic fluid temperature.	col. 5, lines 46-48

Claims	Nature Of Change/Recitation	Supporting text in Patent
209	temperature of the energetic fluid exiting the combustor within a range of about 750 °F to about 2100 °F	Table 3; col. 7, lines 55-60; col. 10, lines 18-30
210	delivery of the fluids is controlled to obtain a desired peak temperature of the energetic fluid near the combustor outlet independent of the rate of energy conversion in the combustor.	col. 6, lines 40-50
211	controlling the flow of thermal diluent fluid in accordance with the flow of oxygen-containing fluid to obtain a desired energetic fluid temperature.	See references relative to claims 119-121.
212	controlling the delivery of thermal diluent to obtain a temperature of the energetic fluid exiting the combustor above about 400 degrees ° C (about 752 ° F).	col. 7, lines 55-60; col. 10, lines 18-30
213	controlling the amount and location of the thermal diluent delivered to obtain a desired fluid temperature and/or a desired fluid temperature profile within the combustor.	col. 9, line 57-col.10, line 37
214	so controlling the delivery of thermal diluent that the maximum combustion temperature is below a desired value.	col. 10, lines 18-30
215	temperature of the energetic fluid exiting the combustor is controlled independently of the enthalpy flow rate of the energetic fluid.	see reference relative to claim 122
216	controlling the delivery of thermal diluent fluid to constrain the temperature of the combusting fluid and/or the energetic fluid thereby to obtain a concentration of nitrogen oxides in the energetic fluid exiting the combustor at or below a desired value.	col. 9, line 57-col. 10, line11

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217	combusting fuel in a first region, etc.	col. 8, line 17- col. 9, line 29
218	controlling the pressure of at least one of the fluids.	patent claim 1 (air pressure)
219, 220	controlling rate of delivery, etc.	Table 3; col. 19, lines 27-28
221	creating turbulence, etc.	col. 5, lines 18-26
222	[removing dissolved materials from the thermal diluent]	col. 22, lines 17-57; col. 24, lines 2-7
223	[fuel-rich combustion in a first location]	col. 9, lines 30-49
224-225	[delivering thermal diluent upstream (and downstream) of the first location]	col. 8, line 17- col. 9, line 29
226	thermal diluent substantially in a gaseous state, and constitutes a substantially larger component of the energetic fluid than the portion of the oxygen-containing fluid in excess of the stoichiometric ratio.	Table 3
227	maintaining the temperature of the energetic fluid below a desired limit while independently controlling the power produced by the utilization device.	see reference to claim 122
228	maintain the temperature of the energetic fluid below a desired limit while independently controlling the rate of thermal energy delivered through the energetic fluid.	see reference to claim 122
229	controlling the concentrations in the energetic fluid of one or more of unreacted oxygen, combustion products, thermal diluent fluid, and components of the oxygen-containing fluid other than oxygen.	col. 17, lines 7-28

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230	controlling the composition and delivery of the thermal diluent fluid such that it has an enthalpy per unit mass greater than that of the oxygen-containing fluid at the fluid temperature and pressure of the energetic fluid exiting the combustor.	col. 17, lines 18-20
231	delivering at least a portion of the available thermal diluent fluid into the combustion chamber; controlling a dwell time for the energetic fluid in the combustor to obtain a desired composition of the energetic fluid exiting the combustor.	col 16, lines 17-42
232	delivering a first portion of the thermal diluent fluid into the combustion chamber . . . controlling a dwell time of the energetic fluid in the combustor, etc.	col. 9, line 57-col. 10, line11
233	the energetic fluid exiting the combustor includes a selected maximum concentration of NO <sub>x</sub> and/or CO.	Table 3
234	controlling the temperature of the energetic fluid to be greater than a desired temperature for at least the dwell time in the combustor.	col. 10, lines 23- 30
235-237	[various utilization devices]	col. 5, lines 1-5
238-241	[various utilization devices]	col. 3, lines 3-13; col. 23, lines 45-49; col. 24, lines 1-12
242	plurality of utilization devices	see reference relative to claim 82
243	desired levels of mechanical and/or thermal power of the utilization device are obtained by controlling the enthalpy flow rate.	see reference relative to claim122

Claims	Nature Of Change/Recitation	Supporting text in Patent
244	controlling the delivery of fluid into and through the combustor in relation the power output of the work engine to maintain the concentration of pollutants in the energetic fluid below a desired level.	col. 17, lines 7-28; Tables 1-3
245	controlling the delivery of fluid into and through the combustor in relation the speed of the work engine to maintain the concentration of pollutants in the energetic fluid below a desired level.	col. 17, lines 7-28; Tables 1-3
246	controlling the delivery of fluid into and through the combustor in relation the energy conversion rate of the utilization device to maintain the concentration of pollutants in the energetic fluid below a desired level.	col. 17, lines 7-28; Tables 1-3
247	retaining combustion products in the combustion chamber for less than or equal to a selected maximum dwell time whereby the concentration of nitrogen oxides in the energetic fluid exiting the combustion chamber	see reference relative to claims 231, 232
248	retaining the energetic fluid in the equilibration chamber for less than or equal to a selected maximum dwell time	see reference relative to claim 232
249	energetic fluid exiting the utilization device contains less than 3 ppm NOx.	col. 19, lines 43-47
250	energetic fluid exiting the utilization device contains less than 3 ppm CO	col. 19, lines 43-47
251	energetic fluid exiting the utilization device contains less than 8 ppm NOx and less than 8 ppm CO.	Table 3

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252	exchanging thermal energy between the oxygen-containing fluid and the thermal diluent fluid prior to combustion.	see reference relative to claim 109
253	heating the thermal diluent fluid before it is mixed with other fluids.	see reference relative to claim 100
254	oxygen-containing fluid is heated by passing it through a heat exchanger thermally coupled to receive heat from the combustion chamber.	see reference relative to claims 100, 102, 109
255	heating oxygen-containing fluid before combustion by transferring heat thereto from the heated thermal diluent fluid.	see reference relative to claims 100, 102, 109
256	heated thermal diluent fluid is mixed with the oxygen-containing fluid upstream of the combustor.	see reference relative to claims 100, 102, 109
257	controlling the delivery of at least one of the fluids independently of the others.	see reference relative to claim 137
258	temperature in the combustor is controlled by delivery of thermal diluent independently of the ratio of oxygen to fuel.	col. 2, lines 14-23; col. 4, lines 28-46, col. 17, lines 7-28; col. 19, line 64 - col. 20, line 27
259	combustion temperature and/or the temperature of the energetic fluid exiting the combustor are controlled independently of the air to fuel ratio.	col. 2, lines 14-23; col. 4, lines 28-46, col. 17, lines 7-28; col. 19, line 64 - col. 20, line 27
260	air to fuel ratio, the combustion temperature, the combustor temperature profile, and the temperature of the energetic fluid near the combustor exit are each controlled independently.	col. 2, lines 14-23; col. 4, lines 28-46, col. 17, lines 7-28; col. 19, line 64 - col. 20, line 27
261	locations at which thermal diluent is delivered to the combustor and the amount of thermal diluent delivered are controlled independently.	col. 2, lines 14-23; col. 4, lines 28-46, col. 17, lines 7-28; col. 19, line 64 - col. 20, line 27

Claims	Nature Of Change/Recitation	Supporting text in Patent
262	temperature of the thermal diluent fluid is controlled independently of the amount of thermal diluent delivered to the combustor.	col. 2, lines 14-23; col. 4, lines 28-46, col. 17, lines 7-28; col. 19, line 64 - col. 20, line 27
263-266	[fuel composition]	col. 6, lines 51-65
267	thermal diluent fluid is water.	col. 2, lines 3-12
268	thermal diluent fluid is substantially entirely water.	col. 2, lines 3-12
269	thermal diluent fluid is water including dissolved solid material.	see reference relative to claim 222
270	oxygen-containing fluid is heated by heat exchange with hot gases exiting the combustor.	see reference relative to claims 100, 102, 109
271	[recovering condensed thermal diluent fluid from a utilization device]	see reference relative to claim 146
272	[recompressing and exhausting un thermal diluent fluid]	see reference relative to claim 146
273	amount of recovered thermal diluent fluid is at least equal to the amount of thermal diluent fluid delivered upstream of the combustor exit.	col. 23, lines 45-67; Tables 1, 2
274	thermal diluent fluid is water.	see reference to claim 148
275	purifying at least part of the recovered thermal diluent fluid before re-delivery to the combustor.	col. 22, line 23
276	recovered thermal diluent fluid is potable water.	col. 22, line 23
277	recovering a portion of the energetic fluid from an outlet of the utilization device; and recirculating the recovered portion of the energetic fluid for re-delivery to the combustor.	col. 22, line 23

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278	recovering at least a portion of the condensed thermal diluent fluid as potable water, etc.	col. 22, line 23
279	potable water is condensed downstream of at least one utilization device	col. 22, line 23
280, 281	removing at least a portion of any non-combustible contaminants contained in the non-potable water.	col. 22, line 23
282	controlling the combustion temperature by independently controlling the delivery of thermal diluent and the ratio of oxygen containing fluid to fuel.	col. 17, lines 7-28; Tables 1-3
283	the temperature of the combustion chamber inner wall is above a desired value.	see reference to claim 157
284	temperature of the energetic fluid exiting the combustor is within a selected range.	Table 3